



# **Ultra-thin Proton Conducting Membranes for H<sub>2</sub> Stream Purification with Protective Getter Coatings**

## **Working Group Meeting Presentation**

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**Margaret Welk**

**Sandia National Laboratories**

**Team: Robert Grubbs, Andrea Ambrosini**



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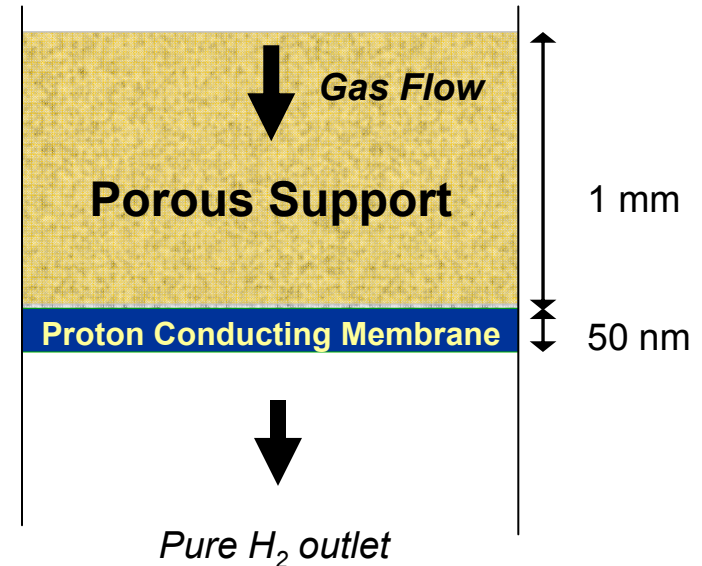




# Overview

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- **Project Objective**
  - Synthesize a proton conducting ceramic (e.g. perovskite) membrane using atomic layer deposition (ALD) techniques
    - Membrane will be thin – 10 to 100 nm
    - Membrane support will be coated with a sulfur getter to deal with contaminants
      - Sulfur getter (e.g. ZnO) will be deposited on the mesoporous alumina support via ALD to conformally coat all surfaces





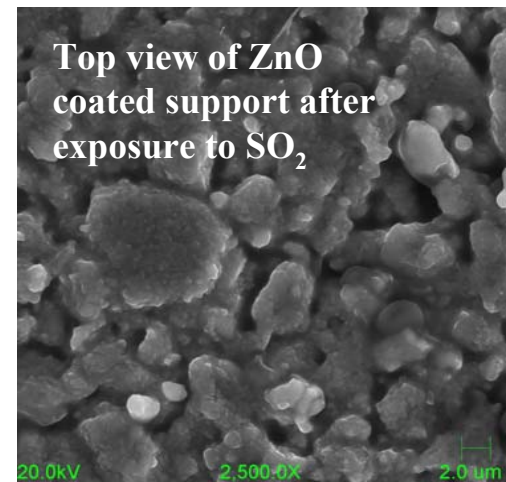
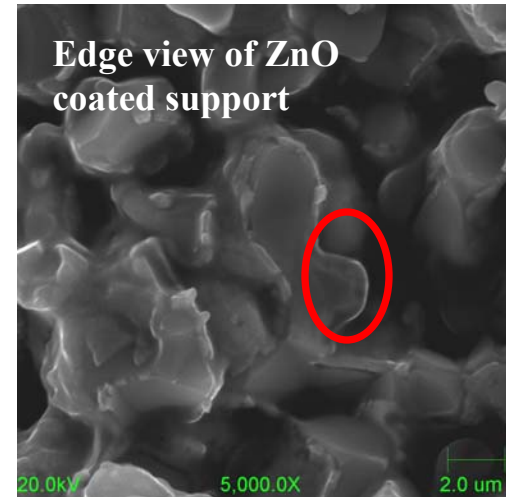
# Work to Date

## Preparatory Work

- Designed permeation unit
- Identified promising ceramic systems –  $\text{SrTiO}_2$  and  $\text{SrCeO}_3$
- Installed oxygen plasma unit for plasma assisted ALD

## Experimental Work

- Deposited ZnO conformally on alumina support
- Confirmed phase of deposited material, measured retained porosity of ZnO coated support
- Studied the results of the conversion of ZnO to  $\text{ZnSO}_4$  after exposure to  $\text{SO}_2$





# Innovation

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- **Couple thin proton conducting membrane with protective “getter” support**
  - **Provide contaminant resistant membrane module**
- **Use ALD and plasma assisted ALD to obtain desired film and coating characteristics**
  - **Excellent control with ALD technique**
  - **Ultra-thin membrane**
    - **Increase flux**
    - **Reduce temperature requirements**
    - **Reduce cost**
  - **Support conformally coated with getter**



# Key Performance Metrics

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## Estimates:

- **Cost per square foot of membrane:** Estimated \$1000 <sup>a</sup>
- **Module cost:** Estimated \$2000 <sup>a</sup>
- **Flux rate:** Current **bulk** ceramic proton conductors = 25 scfh/ft<sup>2</sup> (not thin membranes) <sup>b, c, d</sup>
- **% H<sub>2</sub> recovery:** estimated 50% <sup>b, c, d</sup>
- **Hydrogen quality:** Conduction mechanism produces pure, >99.9% H<sub>2</sub>. Experiments will bear this out. <sup>b, c, d</sup>
- **Operating temperature:** Anticipate 650 to 900°C <sup>b, d</sup>
- **Operating pressure:** Anticipate up to 400 psi. <sup>b, c, d</sup>
- **Durability:** Unknown. Module has the potential for long service life. Dependant on interaction of getter with proton conducting membrane.

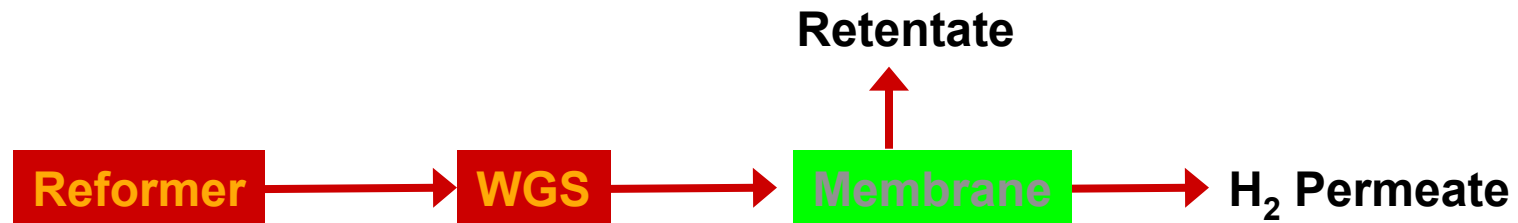
## References:

- Based on unoptimized precursors and deposition parameters.
- Matsumoto, H.; Hamajima, S.; Iwahara, H. Solid State Ionics 145 (2001) 25.
- Shimura, T.; Tokiwa, Y.; Iwahara, H. Solid State Ionics 154 (2002) 653.
- Kokkofitis, C.; Ouzounidou, M.; Skodra, A.; Stoukides, M. Solid State Ionics 178 (2007) 507.



## Summarize Unique H<sub>2</sub>A Inputs

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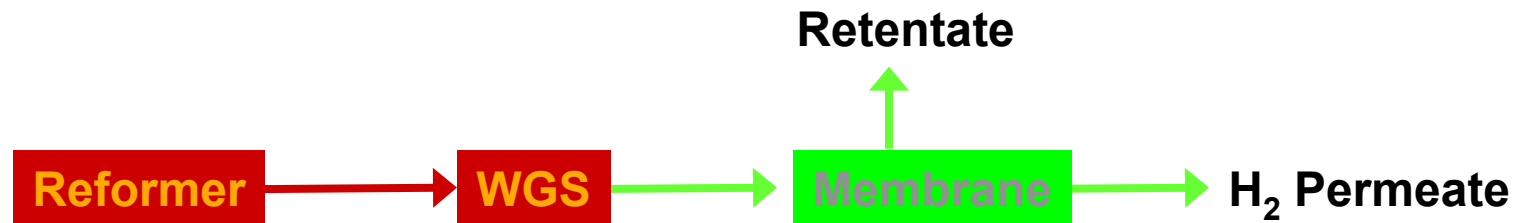


- Ideally will replace part or all of the PSA systems (follow the WGS in a system installation)
- Membrane module will use natural gas feedstocks, and potentially reformed bio-derived feedstocks
- Other energy usage: use co-generated heat and supplement
- Total yearly operating costs: Unknown at this time



# System Definition

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- Will define our system as only the Membrane Module
    - Includes support, membrane and integration structure
- Back of the envelop calculations for **bulk membranes**:
- Capacity: estimated per module 0.15 kg H<sub>2</sub>/day
  - Inputs: reformed natural gas (steam + NG)
  - Outputs: H<sub>2</sub>, retentate consisting of H<sub>2</sub>O, CO, CO<sub>2</sub>, CH<sub>4</sub>, H<sub>2</sub>, periodic regeneration of getter material releases SO<sub>2</sub>.
  - Anticipated size: Targeting desired flux of H<sub>2</sub> size would currently be approximately 20x20x50 cm



## Feed and Energy

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- **Energy input and output of a membrane module**
  - **Characteristics of primary feed:**
    - LHV of natural gas = 930 Btu/ft<sup>3</sup>, or 34.6 MJ/m<sup>3</sup>
      - Reformed NG?
  - **Energy Utilities with usage rate**
    - Unknown
- **Other inputs:**
  - For membrane module, none.





## Other Material Input and Output

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- **Other materials needed**
  - Filter for particulates (part of reforming unit)
  - Purge gas (Air) for getter regeneration
  - Scrubber for sulfur gasses released from regenerated sulfur getter
- **Other outputs:**
  - Retentate will contain CO, CO<sub>2</sub>, H<sub>2</sub>O, H<sub>2</sub>, CH<sub>4</sub>.
  - Regeneration of getter will release SO<sub>2</sub>.



## **Assessment of Status**

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- **Uncertainties in the above information**
  - **All numbers are based on literature values for pressed pellets (~ 1-2 mm thick) of ceramic proton conductors. Until we make and test our first thin membranes (10-50 nm thick) all of these numbers are extremely speculative.**
  - **Operating temperature, flux, operating pressure, and cost estimates may all change significantly. Our first membrane will be tested early next year.**